

**Quiz 7 Chemical Engineering Thermodynamics**  
**February 27, 2020**

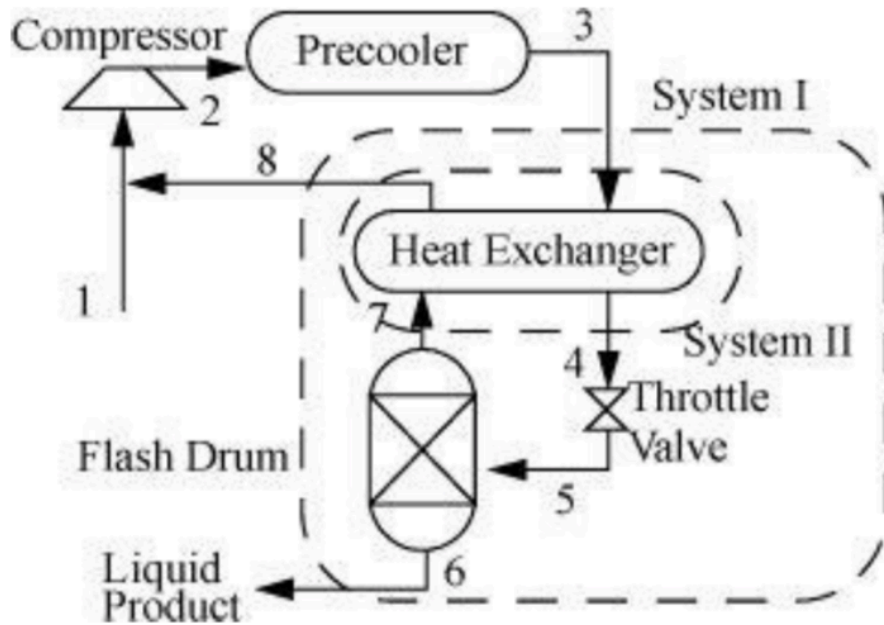
A Linde process is used to produce liquified propane. Stream 3 is at 260K and 6 MPa. Stream 5 is at 0.1 MPa. Streams 8 and 1 are at 295K. Determine all of the missing parameters in the attached table using PREOS.xls. Assume perfect efficiency and no heat loss in the process.

**-For the reference state use an ideal gas with  $H = 0$  at 298K and 0.1 MPa.**

**-Determine all values using PREO.xls.**

In addition to filling out the table:

- 1) Explain the origin of the two equations shown below the diagram.
- 2) What is  $Q_{PC}$  for the precooler?
- 3) What is  $W_s$  for the compressor?
- 4) How is the amount of product  $m_6$  related to  $Q_{PC}$  for the precooler and  $W_s$ ? (Do a balance around the entire process.)



$$q = \frac{H_3 - H_6}{H_8 - H_6}$$

$$H_4 - H_3 = -q(H_8 - H_7)$$

300K is about 80°F

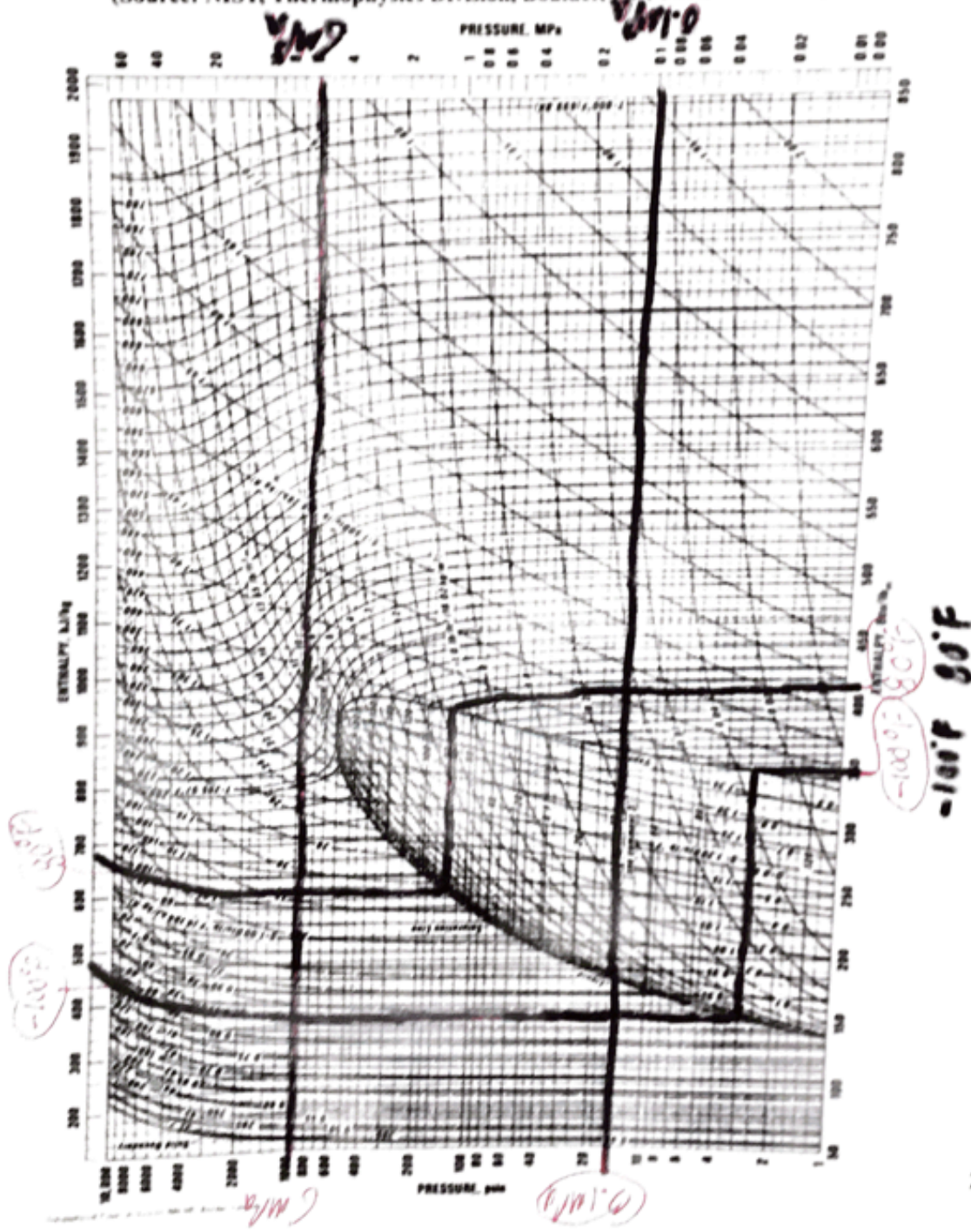
200K is about -100°F

For a perfect compressor, turbine, or pump  $\Delta S = 0$

For a throttle or valve  $\Delta H = 0$

# .11 PRESSURE-ENTHALPY DIAGRAM FOR PROPANE

(Source: NIST, Thermophysics Division, Boulder, CO, USA, used with permission.)



300K is about 80°F 200K is about -100°F

**Reference state ideal gas with  $H = 0$  at 298K and 0.1 MPa**

Stream	State	q	T, K	P, Mpa	V, cm <sup>3</sup> /mole	H, J/mole	S, J/(mole K)
1							
2							
3							
4							
5							
6							
7							
8							

**V = Vapor; L = Liquid; SV = Saturate Vapor ; SL = Saturated Liquid ; V/L = mixed V & L;  
SCF = Supercritical Fluid**

1) Explain the origin of the two equations shown below the diagram.

$$q = \frac{H_3 - H_6}{H_8 - H_6} \quad H_4 - H_3 = -q(H_8 - H_7) \quad (\text{Use another sheet if you need more space})$$

2) What is the value for  $Q_{PC}$  for the precooler?

3) What is the value for  $W_s$  for the compressor?

4) How is the amount of product  $m_6$  related to  $Q_{PC}$  for the precooler and  $W_s$ ? (Do a balance around the entire process.)

Answers Quiz 7 2020

Stream	State	q	T, K	P, Mpa	V, cm <sup>3</sup> /mole	H, J/mole	S, J/(mole K)
1	V	1	295	0.1	24100	-334	-0.988
2	SCF	1	462	6	474	11000	-0.988
3	SCF	1	260	6	74.2	-20300	-87.8
4	SCF	1	254	6	73.2	-20900	-90.2
5	V/L	0.131	231	0.1	2490	-20900	-87.8
6	SL	0	231	0.1	70.9	-23300	-98.4
7	SV	1	231	0.1	18500	-4620	-17.3
8	V	1	295	0.1	24100	-334	-0.988

1) Explain the origin of the two equations shown below the diagram.

$$q = \frac{H_3 - H_6}{H_8 - H_6} \quad H_4 - H_3 = -q(H_8 - H_7) \quad (\text{Use another sheet if you need more space})$$

First from the dashed box that circled streams 3, 6, and 8. Energy balance.  $H_3 = (1-q)H_6 + qH_8$   
 Second from an energy balance on the heat exchanger,  $H_4 - H_3 = -q(H_8 - H_7)$

2) What is the value for  $Q_{PC}$  for the precooler?

$$Q_{PC} = H_3 - H_2 = -20300 \text{ J/mole} - 11,000 \text{ J/mole} = -31,300 \text{ J/mole}$$

3) What is the value for  $W_s$  for the compressor?

$$W_s = H_2 - H_1 \text{ or } H_2 - H_8 = 11,000 \text{ J/mole} + 334 \text{ J/mole} = 11,300 \text{ J/mole}$$

4) How is the amount of product  $m_6$  related to  $Q_{PC}$  for the precooler and  $W_s$ ? (Do a balance around the entire process.)

$$m_6 (H_6 - H_1) = (W_s + Q_{PC})$$

$$m_6 = \frac{(W_s + Q_{PC})}{(H_6 - H_1)} = m_1$$

Use

$$g_5 = \frac{H_3 - H_6}{H_8 - H_6}$$

To get

$$H_4 = -g(H_8 - H_7) + H_3$$

For the table.